IN THE SPECIFICATION

On page 1, above line 1, insert -- Field of the Invention --.

On page 1, above line 24, insert -- Background of the Invention --.

On page 3, above line 13, insert -- Summary of the Invention --.

On page 3, above line 20, insert -- Brief Description of Drawings --.

The invention will now be described by way of example in more detail with reference to the accompanying drawings. The examples should not be construed to limit the scope of the invention.

Figure 1 shows schematically a flow scheme of a liquefaction plant provided with means for carrying out the present invention;

Figure 2 shows schematically an alternative control for the liquefied natural gas product stream; and

Figure 3 shows schematically an alternative embodiment of the invention.--

On page 3, above line 20, insert -- Detailed Description of the Invention --.

On page 4, delete line 32-34.

On page 5, delete line 1-7.

On page 5, above line 8, insert -- Detailed Description of the Drawings --.

On page 18, above line 1, insert -- We claim: --.

2) fully opening the flow control valves, selecting the valve through which, when fully opened, the flow rate of the liquefied natural gas is smallest, and keeping that valve at its fully opened position;

3) determining a dependent set point for the flow rate of the liquefied natural gas flowing through the conduit provided with the other valve such that this flow rate equals the measured flow rate of the liquefied natural gas flowing through the conduit provided with the valve at its fully opened position; and

4) maintaining the flow rate of the liquefied natural gas from the second heat exchanger at its dependent set point.

16. (Original) The method according to claim 15, wherein step 3) comprises determining a dependent set point for the flow rate of the natural gas flowing through the conduit provided with the other valve using the measured flow rates of the liquefied natural gas from the first and second heat exchangers, the flow rates of one of the refrigerants supplied to the heat exchangers, and an operator manipulated set point for the quotient of (i) the ratio of the flow rate of the liquefied natural gas leaving the first heat exchanger to the flow rate of one of the refrigerants supplied to the first heat exchanger and (ii) the ratio of the flow rate of the liquefied natural gas leaving the second heat exchanger to the flow rate that refrigerant supplied to the second heat exchanger.

17. (Original) The method according to claim 15, wherein steps 2), 3) and 4) comprise comparing the measured temperature of the liquefied natural gas from the first heat exchanger to the temperature of the liquefied natural gas from the second heat exchanger; determining the stream having the highest temperature; maintaining the flow rate of the liquefied natural gas stream having the lowest temperature at its operator manipulated set point; determining a dependent set point for the flow rate of the stream having the highest temperature, so as to decrease the temperature of that liquefied natural gas stream; and maintaining the flow rate of that stream at its dependent set point.

18. (New) The method according to claim 15, wherein controlling the flow rate of the liquefied natural gas product stream according to step d) is overridden by determining a dependent set point for the flow rate of the liquefied natural gas product stream such that the temperature of the liquefied natural gas is maintained at an operator manipulated set point.

19. (New) The method according to claim 15, wherein step b) comprises selecting the flow rate of the heavy mixed refrigerant to have an operator manipulated set point, generating a first output signal for adjusting the flow rate of the heavy mixed refrigerant using the operator manipulated set point for the flow rate of the heavy mixed refrigerant, generating a second output signal for adjusting the flow rate of the light mixed refrigerant using (i) the flow rates of the heavy mixed refrigerant and the light mixed refrigerant and (ii) an operator manipulated set point for the ratio of the flow rate of the heavy mixed refrigerant to the flow rate of the light mixed refrigerant.

20. (New) The method according to claim 15, wherein step b) comprises selecting the flow rate of the light mixed refrigerant to have an operator manipulated set point, generating a second output signal for adjusting the flow rate of the light mixed refrigerant using the operator manipulated set point for the flow rate of the light mixed refrigerant, and generating a first output signal for adjusting the flow rate of the heavy mixed refrigerant using (i) the flow rates of the heavy mixed refrigerant and the light mixed refrigerant and (ii) an operator manipulated set point for the ratio of the flow rate of the heavy mixed refrigerant to the flow rate of the light mixed refrigerant.

21. (New) The method according to claim 15, wherein step b) comprises selecting the flow rate of the total mixed refrigerant to have an operator manipulated set point, and generating a first output signal for adjusting the flow rate of the heavy mixed refrigerant and a second output signal for adjusting the flow rate of the light mixed refrigerant using (i) the operator manipulated set point for the flow rate of the total mixed refrigerant, (ii) the flow rates of the heavy and light mixed refrigerants and (iii) an operator manipulated set point for the ratio of the flow rate of the heavy mixed refrigerant to the flow rate of the light mixed refrigerant.

22. (New) The method according to claim 15, wherein the one of the refrigerants in step d) is the heavy mixed refrigerant.

23. (New) The method according to claim 15, wherein the one of the refrigerants in step d) is the light mixed refrigerant.

24. (New) The method according to claim 15, wherein the one of the refrigerants in step d) is the total mixed refrigerant.

25. (New) The method according to claim 15, wherein step d) comprises generating an output signal using (i) an operator manipulated set point for the ratio of the flow rate of the liquefied natural gas product stream to the flow rate of one of the refrigerants and (ii) the flow rate of the one of the refrigerants; generating a second output signal using an operator manipulated set point for the temperature and the measured temperature; and multiplying the output signals with a weighting factor and adding the weighted signals to obtain a dependent set point for the flow rate of the liquefied natural gas product stream.

26. (New) The method according to claim 15, wherein the one of the refrigerants is the heavy mixed refrigerant.

27. (New) The method according to claim 15, wherein the one of the refrigerants is the light mixed refrigerant.

28. (New) The method according to claim 15, wherein the one of the refrigerants is the total mixed refrigerant.

29. (New) The method according to claim 15, wherein the mixed refrigerant used to remove heat from the natural gas is compressed by a compressor driven by a suitable driver, which method further comprises the steps of measuring the power delivered by the driver, and overriding the operator manipulated set point for the flow rate of one of the refrigerants of step

b) if the power has reached a predetermined maximum value, in order that the operator manipulated set point for the flow rate of one of the refrigerants can no longer be increased.

30. (New) The method according to claim 15, wherein the driver is a gas turbine, and wherein the temperature of the gas at the exhaust of the gas turbine is used as a measure of the power of the driver.